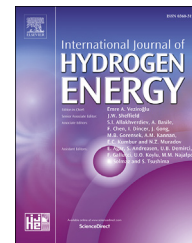




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Hydrogen applications in selective catalytic reduction of NO_x emissions from diesel engines

Ibrahim Aslan Resitoglu ^{a,*}, Ali Keskin ^b

^a Department of Automotive Technology, Mersin University, Technical Sciences Vocational School, TR-33343 Mersin, Turkey

^b Department of Automotive Engineering, Cukurova University, Engineering and Architecture Faculty, TR-01330 Adana, Turkey

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ABSTRACT

Diesel engines have been considered as a major source in nitrogen oxide (NO_x) formation worldwide. The widespread use of diesel engines in consequence of their low fuel consumption, high durability and efficiency increases NO_x emissions day by day. NO_x emissions from diesel engines cause unavoidable damage on environment and people health. Although so many technologies such as exhaust gas recirculation (EGR), lean burn combustion, electronic controlling fuel injection systems, etc. have been developed to control NO_x emissions from diesel engines, they couldn't meet the desired reduction in NO_x emissions. In any case, Selective Catalytic Reduction (SCR) as one of the most promising aftertreatment-emission control technologies is an effective solution in restriction of NO_x emissions. The use of SCR systems especially in heavy-duty diesel powered vehicles has been increasing nowadays. In these systems, to use of hydrogen (H₂) as a reductant or promoter have been improved the conversion efficiency especially at low exhaust temperatures. Many researchers have been focused on the use of H₂ in SCR systems for controlling NO_x emissions.

In this study, the applications of H₂ in SCR of NO_x have been discussed. The studies on use of H₂ in SCR of NO_x emissions were examined and the effects on NO_x conversions were determined. Consequently, it is confirmed that H₂ is a promising and alternative reductant in SCR of NO_x and it has been kept as an attracting subject for many researchers.

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Introduction

NO_x emissions (NO and NO₂) make major contribution to air pollution. They cause many adverse effects on environment and people health [1,2]. Acidification of rain, photochemical smog, greenhouse effect and ozone depletion are the main damages of NO_x on environment while respiratory tract

diseases are the most harmful effect of NO_x on people health [3–5]. Although many sources such as agriculture, thermal plants, industry etc. have been considered as contributor to NO_x emissions, transport sector especially diesel powered vehicles is the main contributor of NO_x emissions [6,7].

Road transport is responsible for around 40% of total NO_x emissions and 85% of NO_x emissions from transport sector are

* Corresponding author. Fax: +9 (0)324 361 0043.

E-mail address: aslanresitoglu@gmail.com (I.A. Resitoglu).

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emitted by diesel-powered vehicles [8,9]. To eliminate NO_x emissions from diesel engines without causing to any decrease in engine performance have been a major barrier for vehicle manufacturers and researchers. To provide this aim, researches have been adopted to SCR technology for diesel vehicles since 2000s and SCR of NO_x emissions from diesel vehicles by urea solution have become one of the most effective methods for vehicles [1,10].

SCR system is currently best choice to eliminate NO_x emissions from diesel engines [7]. NO_x emissions in exhaust gas can be eliminated with a reductant in SCR system [4]. Although different reductants such as alcohols, hydrocarbons, hydrogen, etc. have been sampled, Ammonia (NH₃) is the most commonly used reductant and has high conversion efficiency in SCR of NO_x [6,11]. To prevent the burning of NH₃ in high exhaust temperatures before the reaction, NH₃ is obtained from urea solution [12]. Urea-SCR is the current emission control technology to reduce NO_x emissions from vehicles and other power generating systems. However, many problems such as low activity at low temperatures, ammonia slip, high running cost, NH₃ storage, ash odour, deterioration of catalysts and complex of systems have been direct the researches to alternative SCR technologies [13–16].

Low exhaust temperature is a major problem for urea-SCR applications [17]. At low exhaust temperatures below 200 °C, the reactions of urea solution (thermolysis and hydrolysis) cannot occur properly. Biurea, cyanide acid, ameline, melamine and amelide are constituted due to faulty of reactions [18]. Light off temperature of urea-SCR catalyst is generally around or above 200 °C and NO_x conversion efficiency of urea-SCR is limited at low temperatures [12].

Another SCR technology, the use of HC as reductant in SCR of NO_x, has been worked by many researches currently [19]. Ag/Al₂O₃ is the most promising catalyst type in HC-SCR system [20,21] while V₂O₅-WO₃/TiO₂ catalyst is conventional for urea-SCR system [12]. Compared to urea-SCR, HC-SCR systems provide advantages such as existence of HC in exhaust gas and eliminated the urea tank [19]. However, H₂O vapour leads to significantly decrease in activity of HC-SCR [17].

In urea-SCR and HC-SCR systems, to reduce NO_x emissions at low temperature with high O₂ presentation in exhaust gas is a major problem [22]. The low activities of catalysts at low temperatures have been focused on intensively by many researches for decades. To increase activity at low temperature can be possible to use different reductants or additives.

H₂ has been used in many studies as an alternative fuel for internal combustion engines to eliminate pollutant emissions and improve engine performance [23,24]. The combustion of hydrogen in combustion chamber has improved activity of SCR systems enhancing NO₂/NO_x ratios [25].

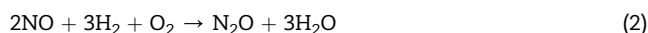
Hydrogen also has been considered as a reductant or promoter in SCR systems for mobile applications [26]. Use of hydrogen in SCR of NO_x emissions has been considered as a green environmental technique because of only H₂O formation following the H₂ combustion. Also high NO_x conversion efficiencies of H₂-SCR at low temperatures have increased the attention of H₂-SCR systems [27]. In this study, the H₂-SCR was explained and the studies on the effects of H₂-SCR on NO_x emissions were discussed.

Use of hydrogen in selective catalytic reduction of NO_x

H₂-SCR system

Generally, H₂ is not used as a reductant in SCR of NO_x. Urea and hydrocarbons are the mainly reductants for SCR reactions. However, hydrogen offers high NO_x conversion efficiency for SCR applications at low temperatures. This advantage makes it to use a promoter [22,28,29] or reductant [13,30,31] in SCR applications. Compared to conventional urea-SCR, H₂-SCR reduces NO_x emissions without forming another pollutants such as biurea, cyanide acid, etc. [1,32]. Fig. 1 presents a typical H₂-SCR system.

H₂-SCR is selective catalytic reduction of NO_x by hydrogen. In H₂-SCR system, H₂ has been choice as reductant agent. It has been used for increasing of NO_x reduction especially at low exhaust temperatures of engine [16]. H₂ is an alternative low temperature (e.g. below 200–300 °C) reductant for SCR systems. Compared NH₃, H₂ is non-corrosive, nontoxic and less processed reductant for SCR applications [33,34]. The reactions occurred in H₂-SCR systems are given in Eqs. (1)–(3) [35,36].



Eq. (1) is the desired reaction which converts NO to N₂. However, Eq. (2) presents an undesired reaction which leads N₂O formation. N₂O is quite harmful and has adverse effects on environment and climate change. It contributes to greenhouse effect more than CO₂. To prevent the formation of NO₂, N₂ selective catalyst must be used. Eq. (3) is the reaction in the oxidation of H₂.

H₂ has an improving effect on catalyst activity and removes the poisonings which restrict the reaction. H₂ supports the formation of NO₂, which is forceful in eliminating of carbon poisoning [37].

The lack of H₂-SCR systems is to supply of H₂ used in SCR of NO_x. The presence of hydrogen in real engine exhaust gas has been in a small amount [38]. So hydrogen has been provided from reliable sources such as tanks and onboard reforming. This option causes increase in costs and safety problems [39].

The use of H₂ in SCR of NO_x has been studied extensively by researchers for a long time. The studies on H₂-SCR systems have been generally based on a small scale with simulated engine emissions in laboratory conditions [10,40,41]. However, a few of researches have been based on a large scale with real diesel engine exhaust gas [26,42,43].

Catalysts and conversion efficiencies of H₂-SCR systems

Supported noble metals are primary choice catalysts in SCR of NO by hydrogen [11]. Noble metals can degrade H₂

actively and degraded H₂ provides NO_x conversion effectively [36]. Pt is the most common noble metal catalyst for H₂-SCR [41]. The reactions initiate with a low light-off temperature about 90 °C over Pt/Al₂O₃ catalyst by the presence of H₂ as reductant [44].

Although Pt based catalysts have high activity at low temperatures, it has high selectivity for N₂O formation and lower selectivity for N₂ [22,31]. However, many studies have been carried out on new catalysts and to improve the N₂ selectivity of Pt based catalyst with reductant of hydrogen under excess oxygen [35].

The type of catalyst substrate (Al₂O₃, SiO₂, ZSM5, etc.) affects strongly the activity of Pt catalyst. Especially the alkalinity and acidity of catalyst has an impact on the dispersion of Pt on catalyst and thus on the activity of catalyst [17]. Expect of Al₂O₃ substrate, different substrate such as; Pt/SiO₂ [45], NiFe_{1.95}Pt_{0.05}O₄ [15], Pt/TiO₂ [46], Pt/MnO_x [34], Pt/Ce_{1-x}Zr_xO_{2-δ} [47] worked in researches. Burch and Coleman [44] compared Al₂O₃ and SiO₂ as Pt catalyst support considering their activity in H₂-SCR. Pt/SiO₂ showed best performance in terms of activity at low temperatures.

The effects of H₂ on selective catalytic reduction of NO over Pt/γ-Al₂O₃, Pd/γ-Al₂O₃ and Ir/γ-Al₂O₃ were studied by Goula et al. [10]. In this research, Pt based catalyst showed higher activity compared to other noble metal based catalysts.

The supplement of WO₃ to Pt/TiO₂ catalysts for H₂-SCR of NO_x investigated by Liu et al. [46]. They found that the supplement of WO₃ led to increase in conversion efficiency at low temperatures. The NO_x conversion efficiency at low temperatures reached up to 90% with the addition WO₃.

Park et al. [45] used zirconia as a main substrate expect conventional alumina and silica in H₂-SCR systems. Pt was used as based noble metal in this study. The results showed that zirconia had better performance as a catalytic support compared alumina and silica in the term of conversion efficiency and hydrothermal stability.

Li et al. [17] tested four different catalysts as, Pt/γ-Al₂O₃, Pt/MgO, Pt/HZSM-5 and Pt/ZrO₂ in H₂-SCR system. They found that conversion efficiency of catalysts were greatly depended on Pt content in catalyst and NO_x adsorption capacity of substrates.

Table 1 shows the activity of different catalyst type in H₂-SCR. In this table, T_{con} is the minimum temperature at which maximum conversion efficiency is obtained. Considering the studies carried out on H₂-SCR catalyst, it is shown that Pt based catalyst is best choice for H₂-SCR applications. NO_x conversions were obtained in high rates at low temperatures almost for all Pt based catalyst.

Clearly, Pd is the most promising catalyst which comes after Pt based catalysts with high conversion efficiencies near the Pt based catalysts. Compared Pt, Pd is remarkable with the specifications of cheaper, high thermal stability, easily available and higher N₂ selectivity [13,52]. Especially the activity of Pd based catalyst in SCR of NO is so high compared to Pt and other noble metal catalysts [53]. Different supports for Pd based catalysts such as Pd–Ir/TiO₂ [33], Pd/K₂O-6TiO₂ [50], Pd/TiO₂-Al₂O₃ [51] performed in H₂-SCR of NO_x by researchers. Qi et al. [5] used H₂ as a reductant to catalytic reduction of NO_x with Pd catalysts. They found that H₂ gave high NO conversion at low temperatures with Pd catalysts.

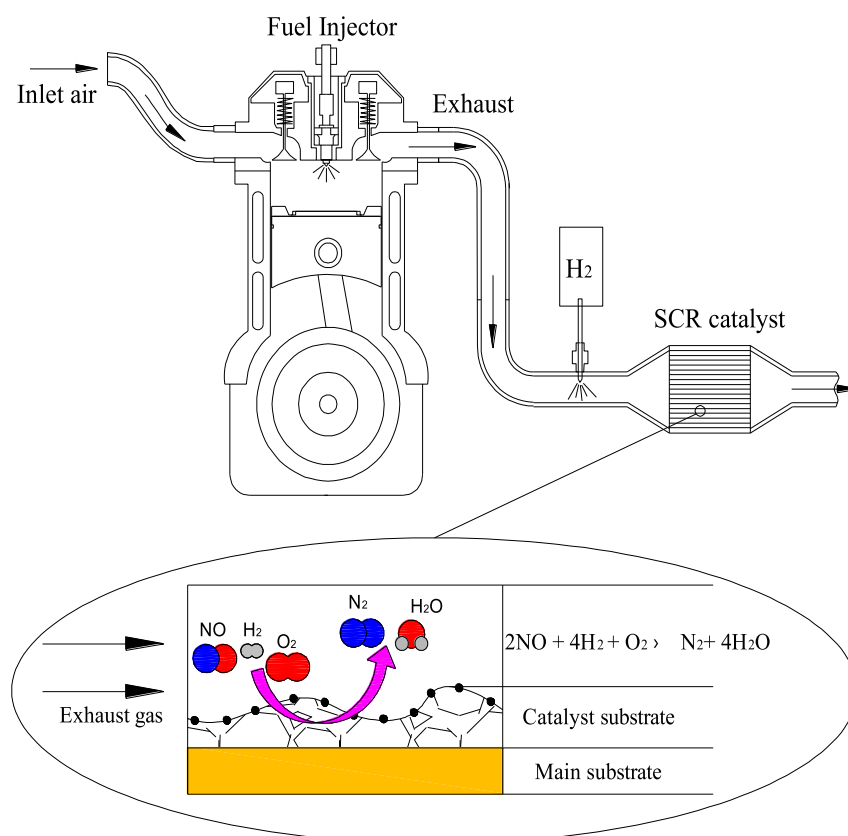


Fig. 1 – Selective catalytic reduction of NO by hydrogen.

Table 1 – Different catalyst type used in H₂-SCR applications.

Catalyst	Gas concentrations				~T _{con.} (°C)	~ Max. NO conversion (%)	Ref.
	H ₂	O ₂ (%)	NO	GHSV (h ⁻¹)			
%1 Pt/Al ₂ O ₃	0.8%	5	480 ppm	–	50	100	[45]
0.5% Pt/Al ₂ O ₃	2000 ppm	6	500 ppm	22,000	80	82	[41]
0.5% Pt/γ-Al ₂ O ₃	0.5%	2	1000 ppm	40,000	120	93	[10]
%1 Pt/SiO ₂	0.8%	5	480 ppm	–	100	98	[45]
%0.5 Pt/TiO ₂	1%	5	0.25%	53,000	200	82	[46]
%0.5 Pt/2% WO ₃ /TiO ₂	1%	5	0.25%	53,000	125	88	[46]
Pt/ZSM5	1000 ppm	–	1000 ppm	60,000	100	100	[48]
1% Pt/ZSM35	0.5%	6.7	1%	80,000	120	80	[40]
1% Pt/Beta	0.5%	6.7	1%	80,000	115	55	[40]
0.3 Pt/ZrO ₂	2000 ppm	6	500 ppm	22,000	150	95	[41]
Pt/Si-MCM	5000 ppm	6.7	1000 ppm	80,000	100	60	[49]
0.95% Pd/Al ₂ O ₃	5000 ppm	5	1000 ppm	60,000	125	55	[50]
0.94% Pd/TiO ₂	5000 ppm	5	1000 ppm	60,000	100	60	[50]
1.9% Pd/TiO ₂	3000 ppm	5	1000 ppm	60,000	375	40	[33]
%1 Pd/TiO ₂ -Al ₂ O ₃	4000 ppm	5	500 ppm	–	150	98	[51]
1.8% Rh/TiO ₂	3000 ppm	5	1000 ppm	60,000	550	35	[33]
Rh/ZSM5	1000 ppm	–	1000 ppm	60,000	300	100	[48]
1.7% Ir/TiO ₂	3000 ppm	5	1000 ppm	60,000	475	65	[33]
0.5% Ir/γ-Al ₂ O ₃	0.5%	2	1000 ppm	40,000	340	16	[10]
NiFe ₂ O ₄	10,700 ppm	2	1070 ppm	23,400	220	42	[32]
NiFe _{1.95} Pd _{0.05} O ₄	10,700 ppm	2	1070 ppm	23,400	190	100	[32]
NiCo ₂ O ₄	10,700 ppm	2	1070 ppm	48,000	350	40	[1]
NiCo _{1.95} Pd _{0.05} O ₄	10,700 ppm	2	1070 ppm	48,000	200	92	[1]
Co/ZSM5	1000 ppm	–	1000 ppm	60,000	500	100	[48]
Cu/ZSM5	1000 ppm	–	1000 ppm	60,000	600	90	[48]
CoFe ₂ O ₄	10,000 ppm	2	1000 ppm	23,400	250	84	[32]
CoFe _{1.95} Pd _{0.05} O ₄	10,000 ppm	2	1000 ppm	23,400	170	95	[32]

Except Pt and Pd, different catalysts such as Rh, Ni, Ir, TiO₂, Co, etc. have been developed by researchers as alternative catalysts for H₂-SCR applications. Xu et al. [13] developed NiFe_{2-x}Pd_xO₄ catalysts for the SCR of NO by hydrogen. They obtained nearly 100% NO conversion at 190 °C. In their other study [27], they searched the effect of aluminate spinel oxides (CuAl₂O₄, CoAl₂O₄, ZnAl₂O₄) and palladium-substituted aluminates (CuAl_{1.95}Pd_{0.05}O₄, CoAl_{1.95}Pd_{0.05}O₄, ZnAl_{1.95}Pd_{0.05}O₄) on H₂-SCR of NO. Palladium-substituted aluminates showed better activity compared to aluminate spinel oxides under the same reaction conditions. Approximately maximum conversion efficiency was obtained as 95% with CoAl_{1.95}Pd_{0.05}O₄.

H₂ assisted HC-SCR system

H₂ has been also used as promoter in HC-SCR systems. H₂ improves conversion efficiency of HC-SCR affecting catalyst and other reactants [39]. Especially at low temperature, the supplement of H₂ into exhaust gas increase catalyst activity [54]. Many researches have been carried out on H₂ assisted HC-SCR systems. Ag/Al₂O₃ has been most common catalyst in these researches due to its high activity and efficiency in SCR of NO by hydrocarbons [55]. Except Al₂O₃, different supports like MFI zeolite [29,56] have been used in Ag based catalyst for H₂ assisted HC-SCR.

Abu-Jrai and Tsolakis [42] studied the effect of H₂ and CO addition on HC-SCR activity over 1% Pt/Al₂O₃. Unlike other studies they performed their study using real diesel engine exhaust gas. H₂ addition improved the HC-SCR activity at low temperatures between 100 °C and 300 °C. Another study on

the effect of hydrogen on the efficiency of NO_x reduction with HC-SCR was carried out by Gu et al. [43] using both laboratory and engine test-bench. They preferred Ag/Al₂O₃ catalyst in their research because of its high performance for HC-SCR applications. Results showed that H₂ had an improving effect on NO_x conversion at both laboratory condition and real working situation. NO_x conversion rates increased up to three times with the use of H₂ in the tests carried out on engine test-bench. Shimizu et al. [29] investigated the hydrogen effect on HC-SCR. Ag-MFI was used as catalyst in this experimental study. The use of hydrogen led to increase the coverage of surface intermediates, NO₂ concentration and N₂ formation.

The hydrogen effect on SCR of NO by propane over Ag/Al₂O₃ catalyst was investigated by Richter et al. [57]. They found that the propounding of H₂ avoid to NO conversion to NO₂ form substantially. The presence of H₂ raised the NO_x conversion up to 60% from marginal conversion rates.

Theinnoi et al. [58] searched the effect of H₂ promotion on passive HC-SCR activity. They performed their study over Ag/Al₂O₃ catalyst promoting H₂ (500–3000 ppm) with real diesel exhaust gas. Consequently, they reached two results for H₂ effects on silver catalysis. These results were the increase in initial activity and the decrease in deactivation rate of catalyst.

Sadokhina et al. [2] searched the catalytic activity of Ag/Al₂O₃ catalyst in SCR of NO_x in the presence of small amount of H₂. In this experimental study, the addition of ~1000 ppm hydrogen improved activity and selectivity of catalyst.

Zhang et al. [59] searched the effect of hydrogen on reaction intermediates in the selective catalytic reduction of NO_x

by C_3H_6 . Ag/Al_2O_3 was preferred as catalyst in their study since its high NO_x conversion efficiency by alcohols. They found that the addition of H_2 was significantly increased NO_x conversion at low temperature range of 200–350 °C.

Stakheev et al. [60] investigated the effects of H_2 addition amount on HC-SCR of NO_x over Ag/Al_2O_3 . They used different H_2 amounts from 0 to 1600 ppm in their researches. Consequently, NO_x conversion showed increase in direct proportionally with H_2 addition amount.

Conclusions

This review focused on H_2 applications in SCR technology. The H_2 -SCR technology was expressed and the researches on H_2 -SCR was scrutinised in this study. The researches carried out on H_2 -SCR showed that the addition of hydrogen resulted in conversion of the oxidized nitrogen to N_2 on the catalyst surface. H_2 has an improving effect on SCR activity especially at low temperature. Pt and Pd based catalysts are the most feasible and current for H_2 -SCR applications while Ag based catalysts have high efficiency in H_2 assisted HC-SCR applications. The most of researches on H_2 -SCR have been carried out in laboratory conditions. The studies carried out in real working conditions of engine are substantially restricted. Investigations in real working situations must be increased with future studies. In conclusion, H_2 is a promising reductant for SCR applications of NO_x without caused any formation of pollutants and the researches on improving of H_2 -SCR will continue for a longer time.

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